

# GAS TREATMENT FOR REMOVAL OF HYDROGEN SULFIDE AND SILOXANES

Presentation to WEF R2E Group

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### HYDROGEN SULFIDE (H<sub>2</sub>S) Notes:

#### **Gas Concentrations:**

- Depends on feed to anaerobic digester, or wastes accepted at landfill
- Anaerobic digester concentrations from 100 ->10,000 ppmv
- Landfill 50 5000 ppmv

#### **Properties:**

- Heavier than air gas with low TLV/SEL
- Liquid/Gas Partitioning:
  - Present in liquid as an ion or a dissolved gas:
    - $Ka/[H^+] = [HS^-]/[H_2S]$
    - pKa = 7.1 (25C)
  - Henry's Law:
    - $[HS-] = K_h * P(H_2S)$
    - $K_h = 0.1 \text{ mol/L-atm}$





#### Technologies by H<sub>2</sub>S Loading:

- Activated Carbon Adsorption
- Chemical Scrubbing
- Sacrificial Media
- Biological Conversion to Sulfate
- Biological Conversion to S<sub>o</sub>
- Proprietary Gas/Liquid Contact
- Electrolysis (New)



#### SACRIFICIAL MEDIA SYSTEMS

#### **Media Types:**

- Iron Sponge (Varec, Shand & Jurs, ...)
- Enhanced Fe Sponge (MV Tech)
- Iron Oxide Coated Substrate (Sulfa Treat, Axens, ...)
- FeOH Media (Unison, Ferrosorp)

#### **Modeling / Changeout Considerations:**

- Gas flow, H2S concentration and effluent concentration
- Gas moisture and oxygen concentration
- Form of spent media (loose vs clumps)
- Exothermic temperature rise after media removal

## H<sub>2</sub>S MEDIA EXAMPLE









#### BIOLOGICAL TREATMENT SYSTEMS

#### **Conversion to Sulfate:**

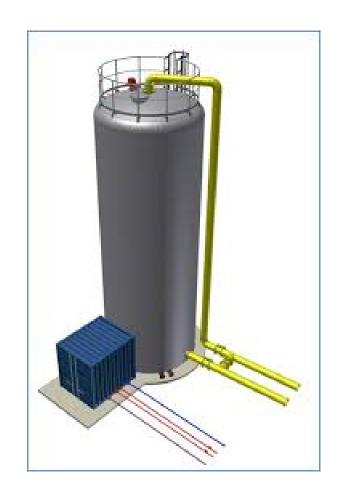
- Range and variability of loading
- Potential polish media for high concentrations and low effluent required
- Neutralization of wastewater
- Dilution of product gas (for high inlet concentration)

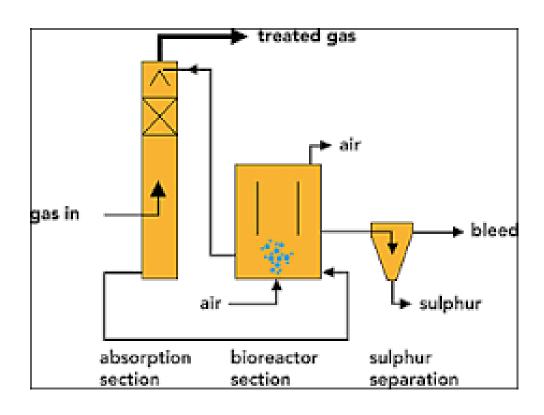
#### Conversion to S<sub>o</sub>:

- Range and variability of loading
- Potential polish media for high concentrations and low effluent required
- Larger space required
- Dewatering of waste, potential
   S<sub>o</sub> reuse



## BIOLOGICAL H<sub>2</sub>S TREATMENT







Melting

Boiling

Vapor

#### SILOXANE TREATMENT

## Degree of Treatment Based on Fuel Use:

- Medium efficiency reciprocating engines
- Turbine with recuperator
- High efficiency reciprocating engines
- Microturbines
- CHG / RNG
- Emission control catalyst

#### **Varying Physical Properties:**

				Vapoi	Doming	Wichting
				Pressure	Point	Point
	Compound	Abbreviation	MW	mmHg, 77F	٥F	٥F
J	Trimethylsilyl fluoride		92.19	760	60.8	-101.2
	Ethoxytrimethylsilane		118.25	400	165.2	-117.4
	Isopropoxytrimethylsilane		132			
	Propoxytrimethylsilane		132	40.2	214.88	32
	Hexamethylcyclotrisiloxane	D3	222	10	275	147
	Octamethylcyclotetrasiloxane	D4	297	1.3	348	63
	Decamethylcyclopentasiloxane	D5	371	0.4	412	-47
	Dodecamethylcyclotrisiloxane	D6	445	0.02	473	26.6
	Hexamethyldisiloxane	L2, MM	162	31	224	-88.6
	Octamethyltrisiloxane	L3, MDM	236	3.9	307	-115.6
	Decamethyltetrasiloxane	L4, MD2M	310	0.55	381	-90.4
	Dodecamethylpentasiloxane	L5, MD3M	384	0.07	446	-113.8
	Trimethylsilanol	TMS	90	19	210	10.4
	Tetramethylsilane		88.2	11.66	82	-187





#### **Non-Regenerable Systems**

- Activated carbon adsorption
- Silica gel adsorption
- Refrigeration systems
- Treatment capacity can be influenced by H<sub>2</sub>S or VOC loading

#### **Regenerable Systems**

- Temperature swing adsorption
- Requires regen flare
- Media ranges from activated alumina to molecular sieve
- Can be followed by AC or 2<sup>nd</sup> regen system

## REGENERABLE EXAMPLES



