

A Simple and Energy Efficient Approach to Cleaning Biogas

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CSWEA WI Section Operations Seminar: Resource Recovery

October 31, 2017



Outline

- Background
- MMSD Pilot
- Summary and Next Steps



Outline

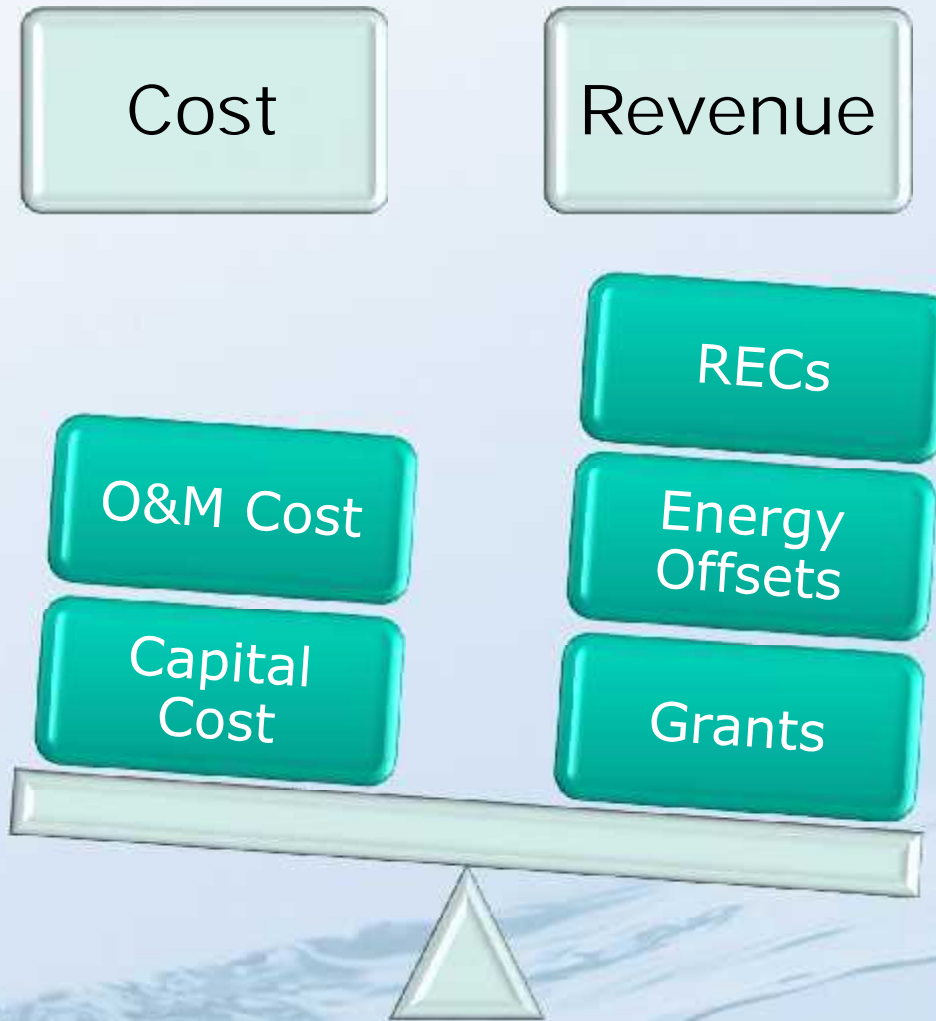
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Biogas projects provide multiple benefits

- Generate renewable fuel with a low carbon content
- Reduce reliance on fossil fuel
 - Reduce greenhouse gas (GHG) emissions
 - Reduce local air pollutant emissions
- Reduce the use of synthetic fertilizers
 - Generate a soil amendment
 - Offset fossil fuel use and reduce GHGs emissions from fertilizer manufacturing
- Help achieve Federal and state goals

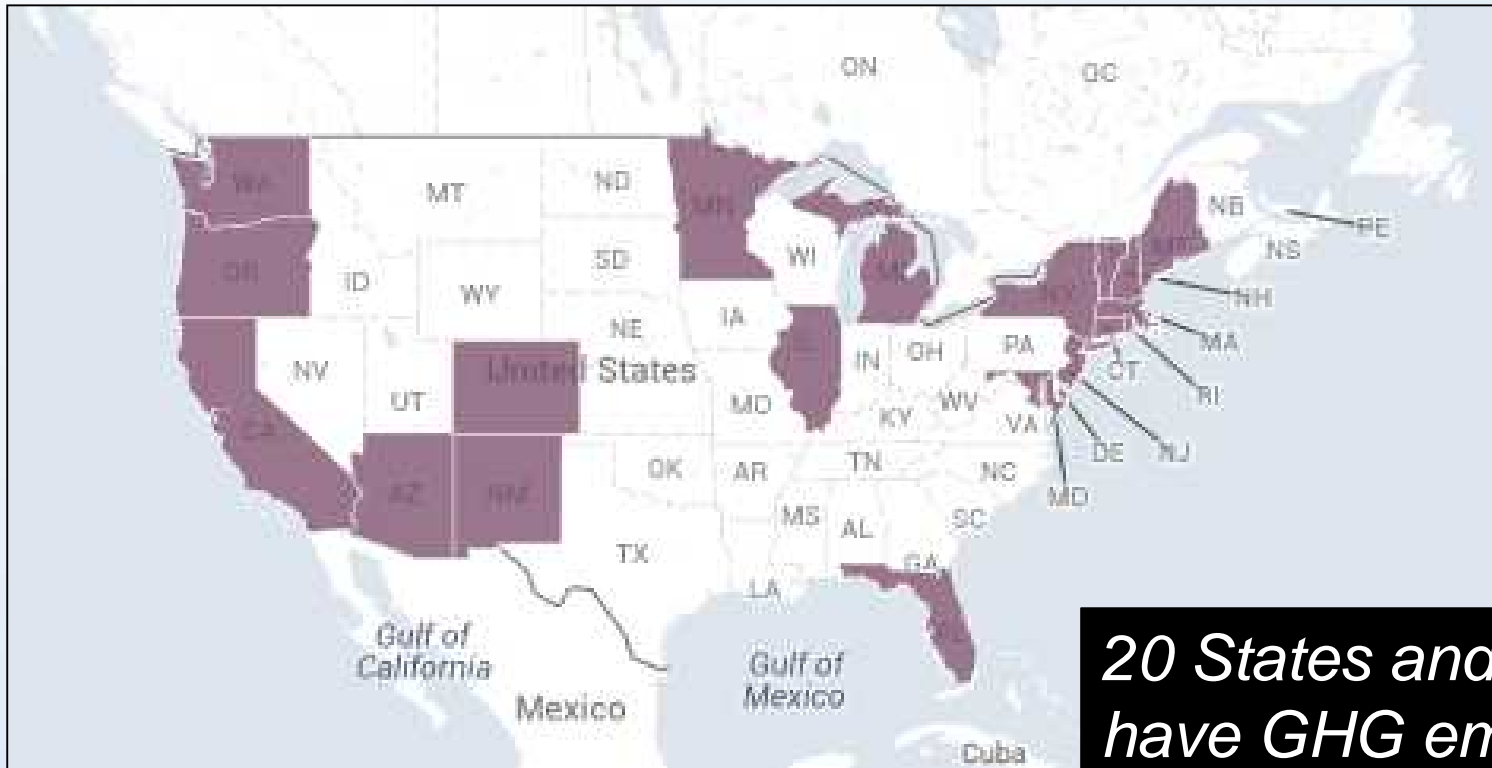
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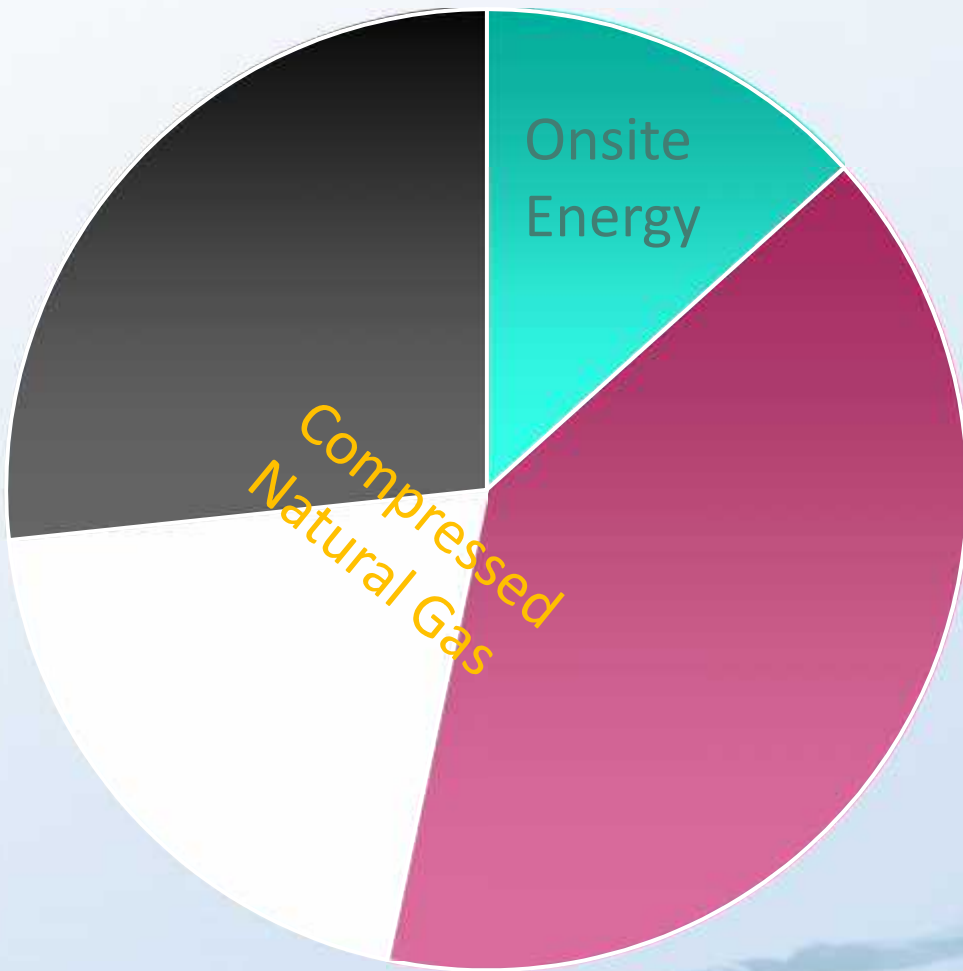
Many states have climate change related goals that incentivize bioenergy projects



20 States and D.C. have GHG emissions reduction targets and associated goals

<https://www.c2es.org/us-states-regions/policy-maps>

Incentives for production/use of biogas are increasing...



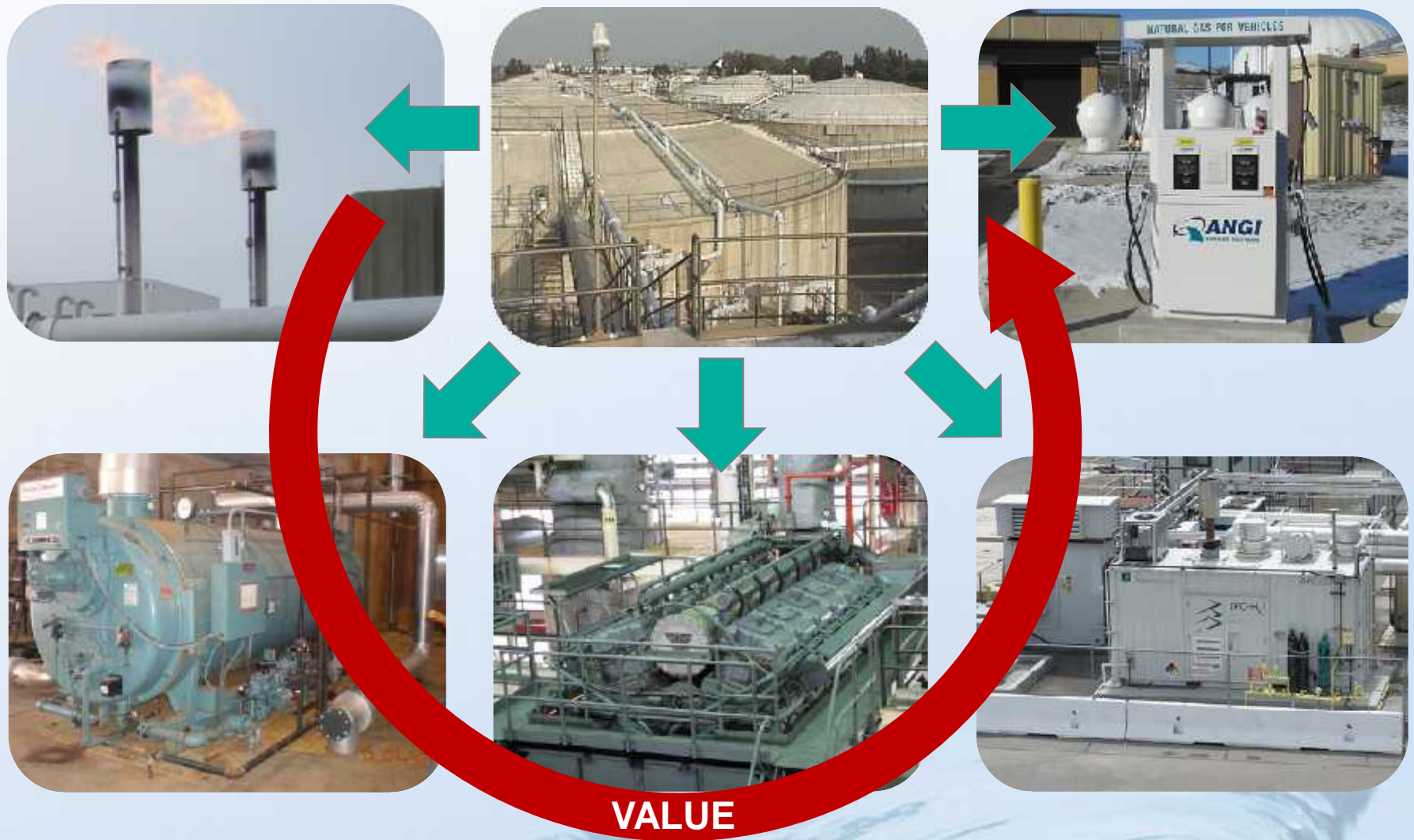
- Renewable Energy Credits
- Renewable Fuel Standard
- Low Carbon Fuel Standard
- Alternative & Renewable Fuel & Vehicle Technology

Cost

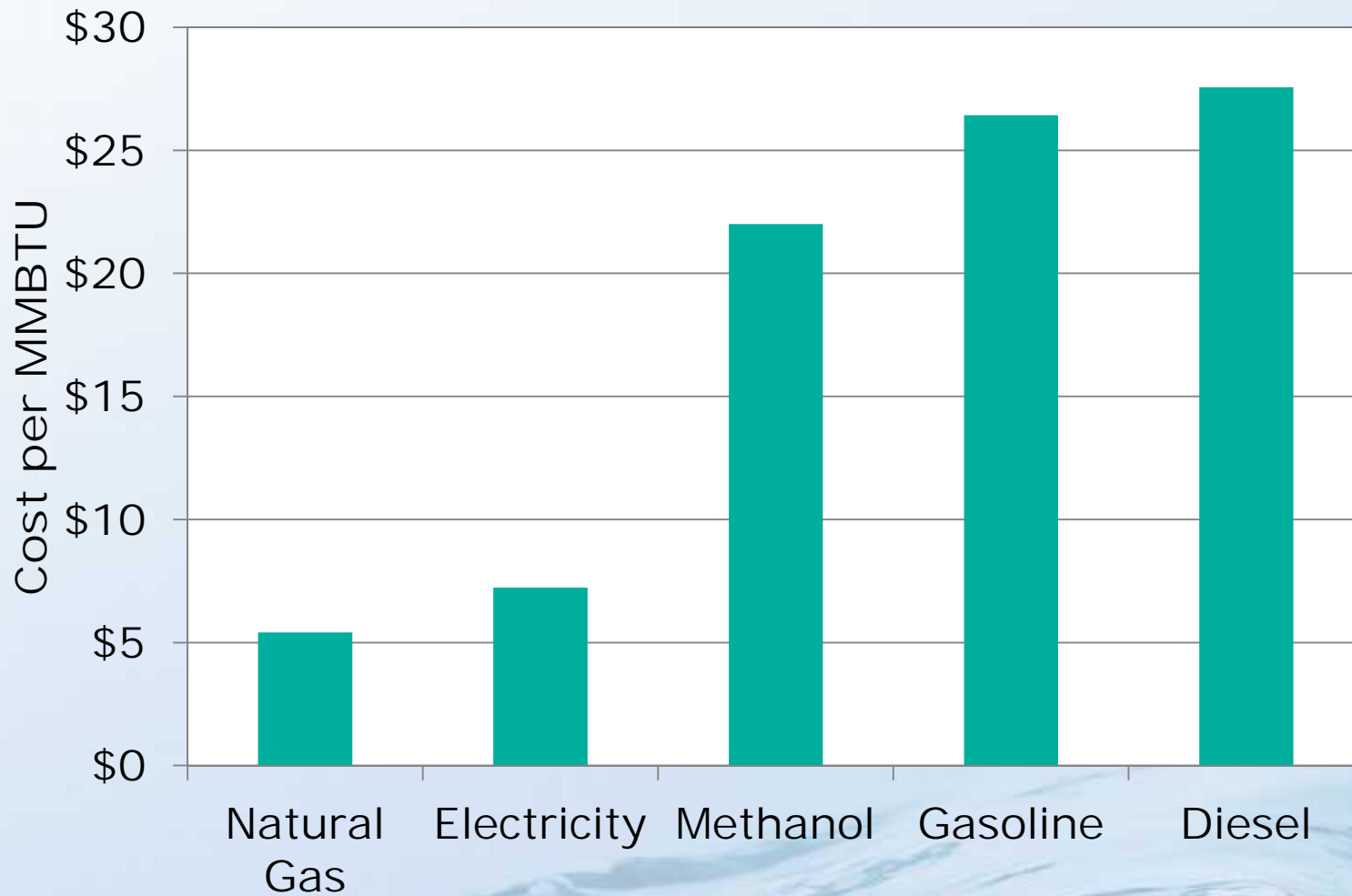
Revenue



Beneficial biogas use offsets fuel costs

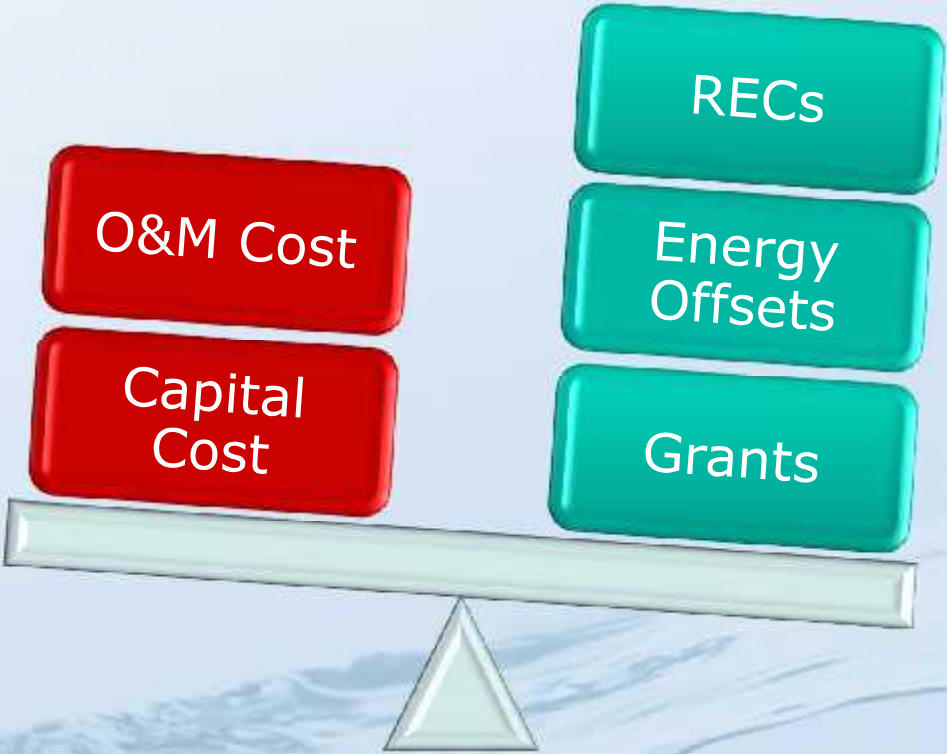


The value of biogas depends on what fuel it is offsetting



Cost

Revenue



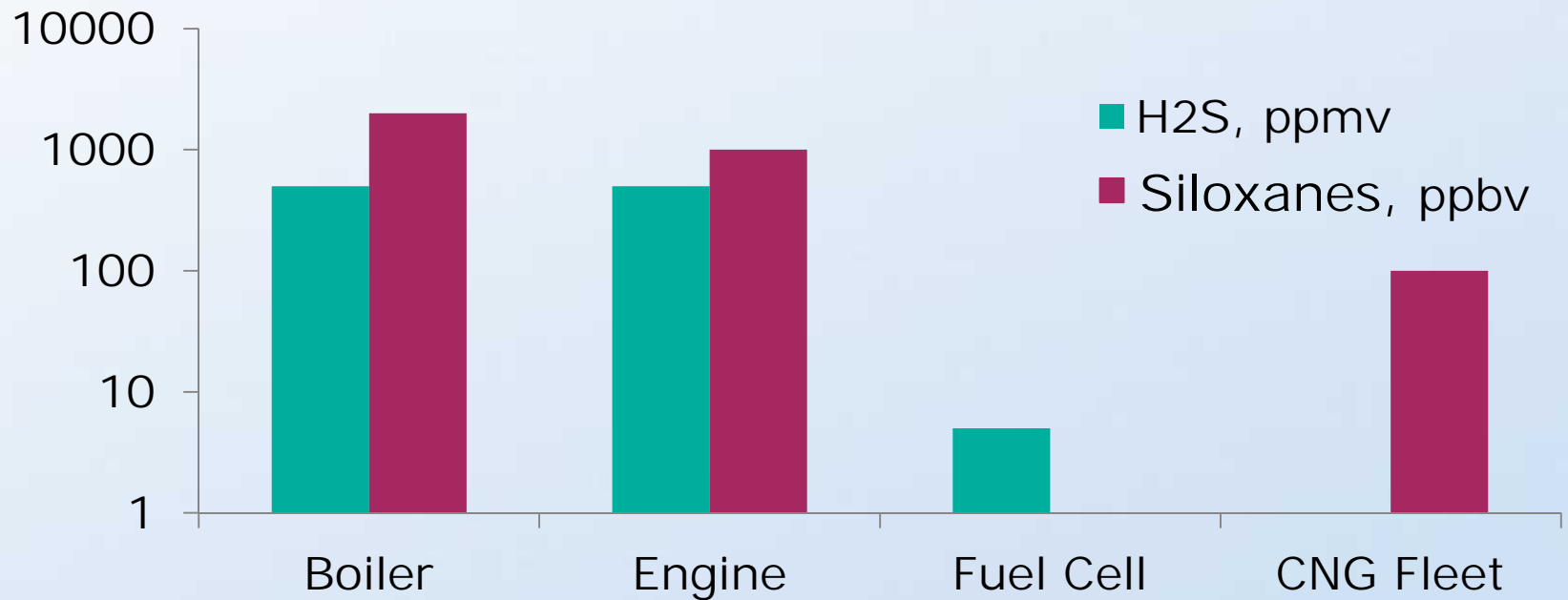
Biogas conditioning is an important component for beneficial use

Parameter	Typical Range
Methane, % by volume	50 – 65
CO ₂ , % by volume	35 – 50
H ₂ S, ppmv	100 – 10,000
Siloxanes, ppbv	500 – 5,000

H₂S and siloxanes damage mechanical equipment

CO₂ reduces energy value and increases compression cost

The level of biogas treatment depends on the type of beneficial use



Commercial biogas treatment can be achieved through different processes

- H₂S removal
 - Iron salt addition
 - Adsorption systems
 - Caustic scrubbers
- Siloxane removal
 - Chillers
 - GAC systems
- CO₂ removal
 - Pressure swing adsorption

New Unison biogas scrubber addresses industry challenges

- Removes H₂S
- Removes CO₂
- Reduces siloxanes
- Chemical-free treatment for digester gas
- No moving parts
- Only uses water



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South Shore Water Reclamation Facility

NACWA Platinum Award 20



**300 MGD Full
Treatment Capacity**
90 MGD Annual Average

Liquid Treatment Processes

- Preliminary/Primary/
Secondary/Disinfection
- Chemical P removal

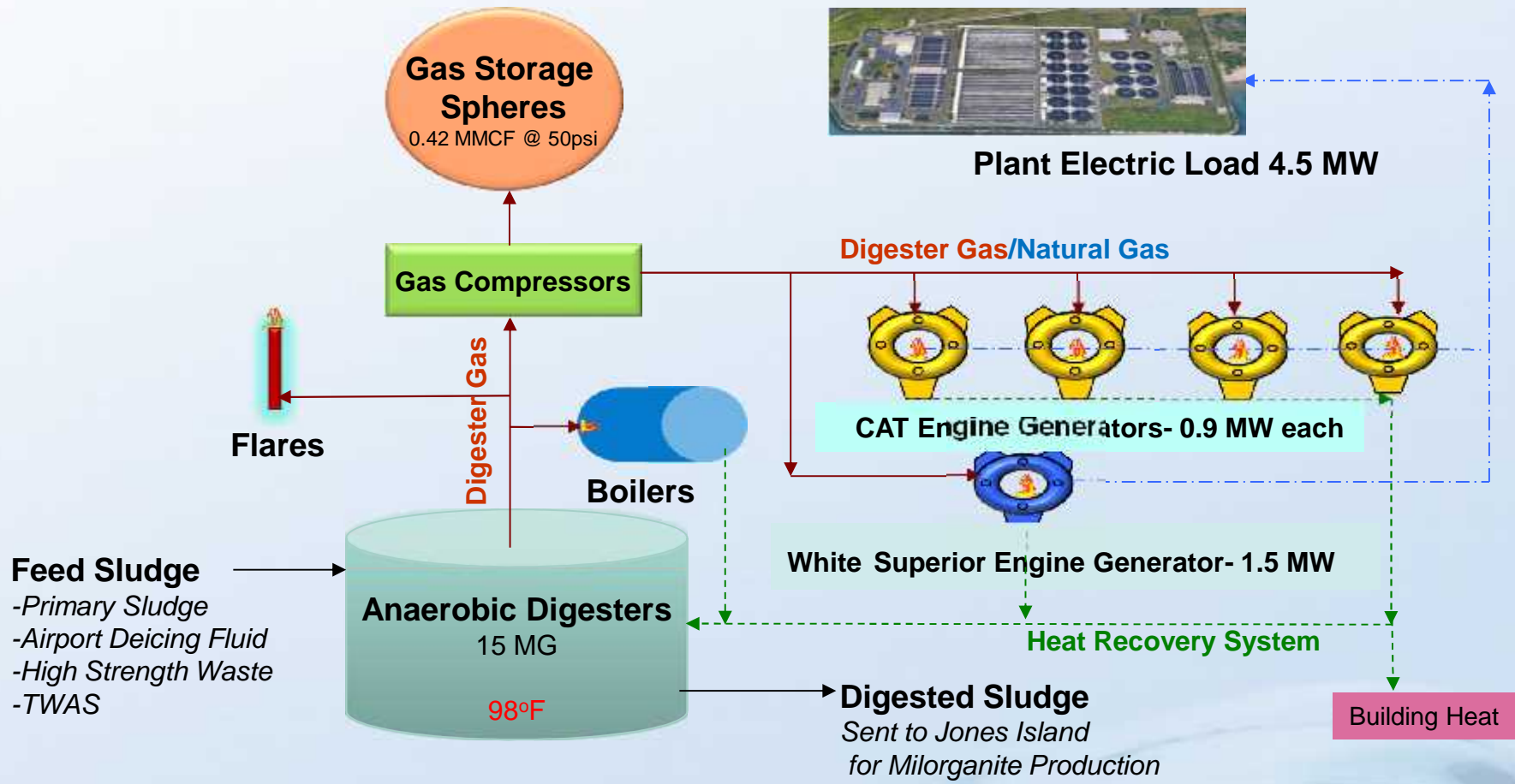
Solids Handling & Disposal

- Interplant pumping of
solids
- GBTs and Plate and
Frame
- Digesters Methane 1.3
MMCF

South Shore Digester Gas Production and Utilization



Plant Electric Load 4.5 MW



South Shore Digester Gas Quality and Quantity

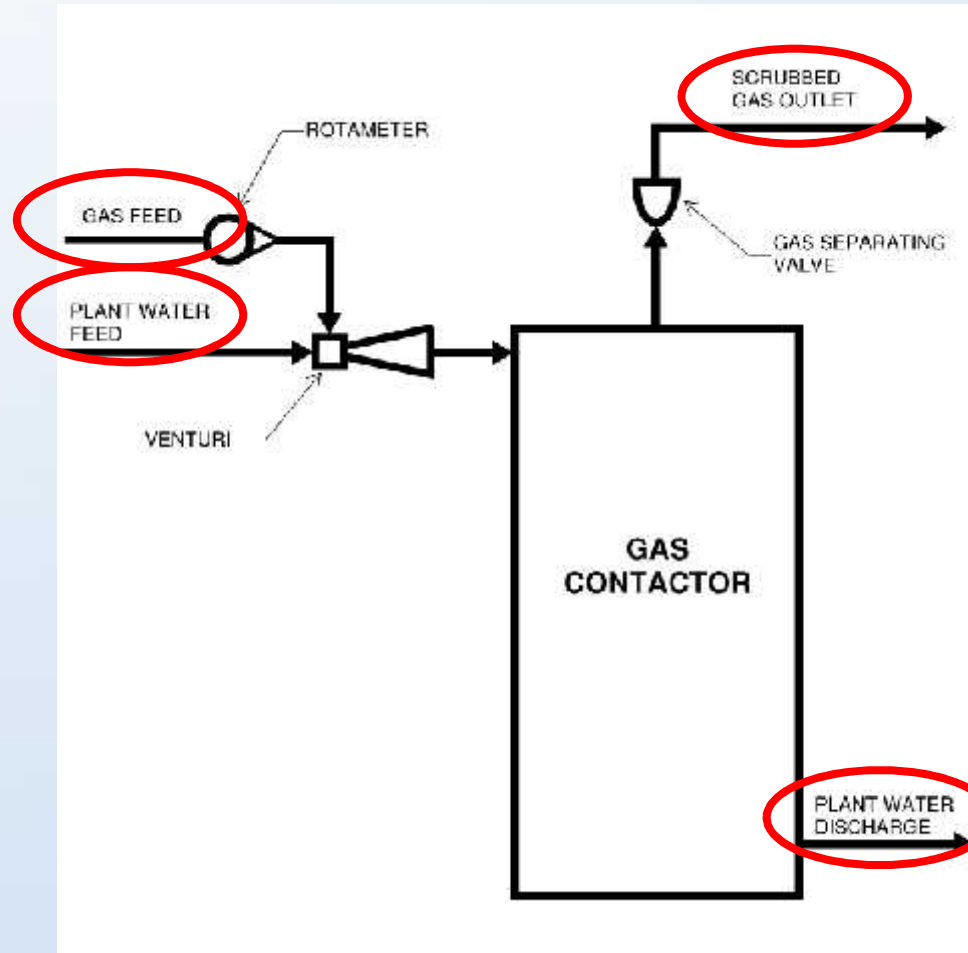
MMSD Plant Data⁽¹⁾

Information Item	Unit	Average	Maximum	Notes
Quantity of digester gas available to be treated	Scf/Day	1,320,000	2,120,000	
Gas Quality:				
• Methane	%	59	63	
• Low Heat Value	Btu-LHV/scf	530	565	
• Carbon Dioxide	%	33.2	38	
• Hydrogen Sulfide (ppm)	ppmv	21.7	34.9	Iron added to primary influent
• Total Siloxanes	mgSi/Nm ³ CH ₄	22.16	320	Concentration Si in methane fraction
• Total Siloxanes	mgSi/Nm ³	13.28	202	Concentration in digester gas

Notes:

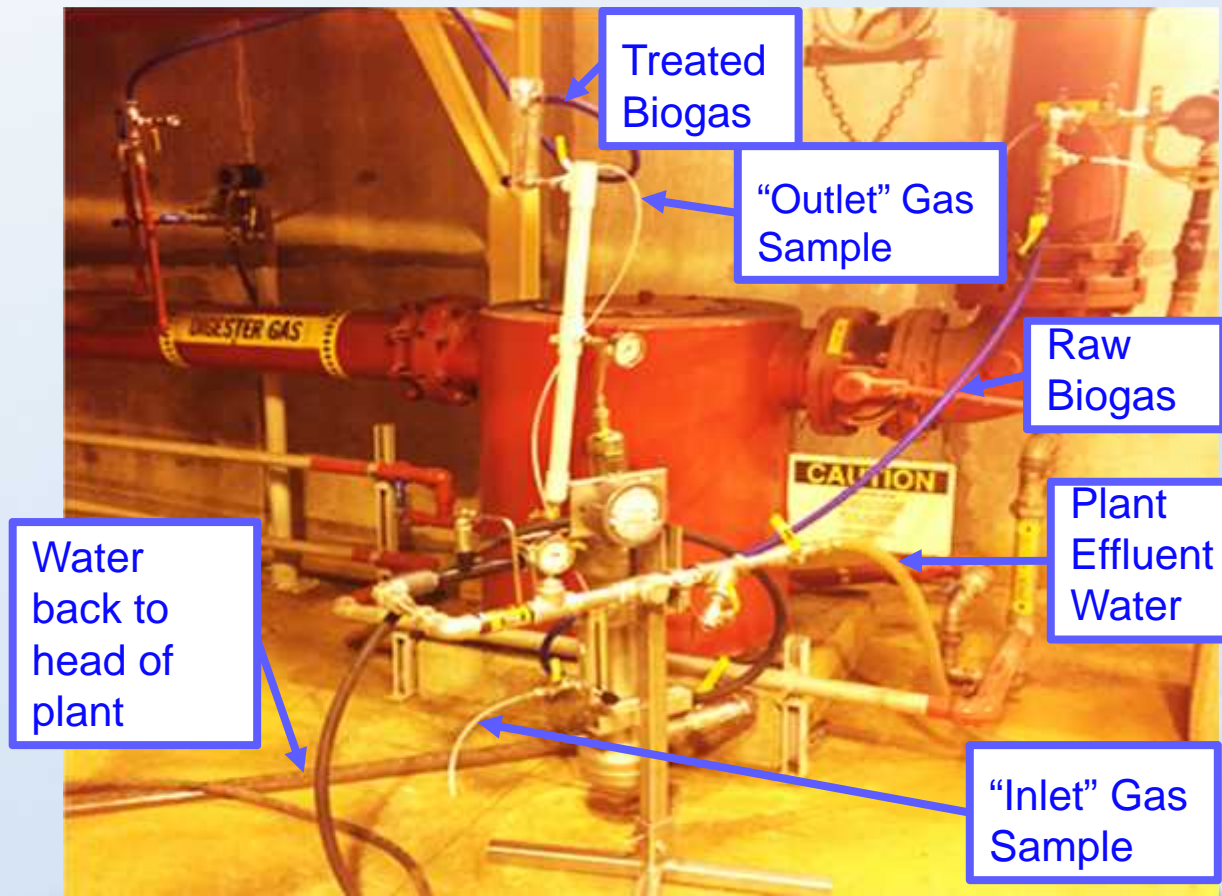
(1) Based on 2014-2016 data.

The technology itself is simple



Pilot Unit Setup

- Located in digester gallery of South Shore WRF



Venturi and Gas Contactor/Moisture Separator



- Plant Effluent Water Used
- Inlet water Pressure 30 psig
- Discharge water pressure= 4 psig
- Water Inlet Flow = 12 gpm

Inlet Outlet Reading Hand Held Device

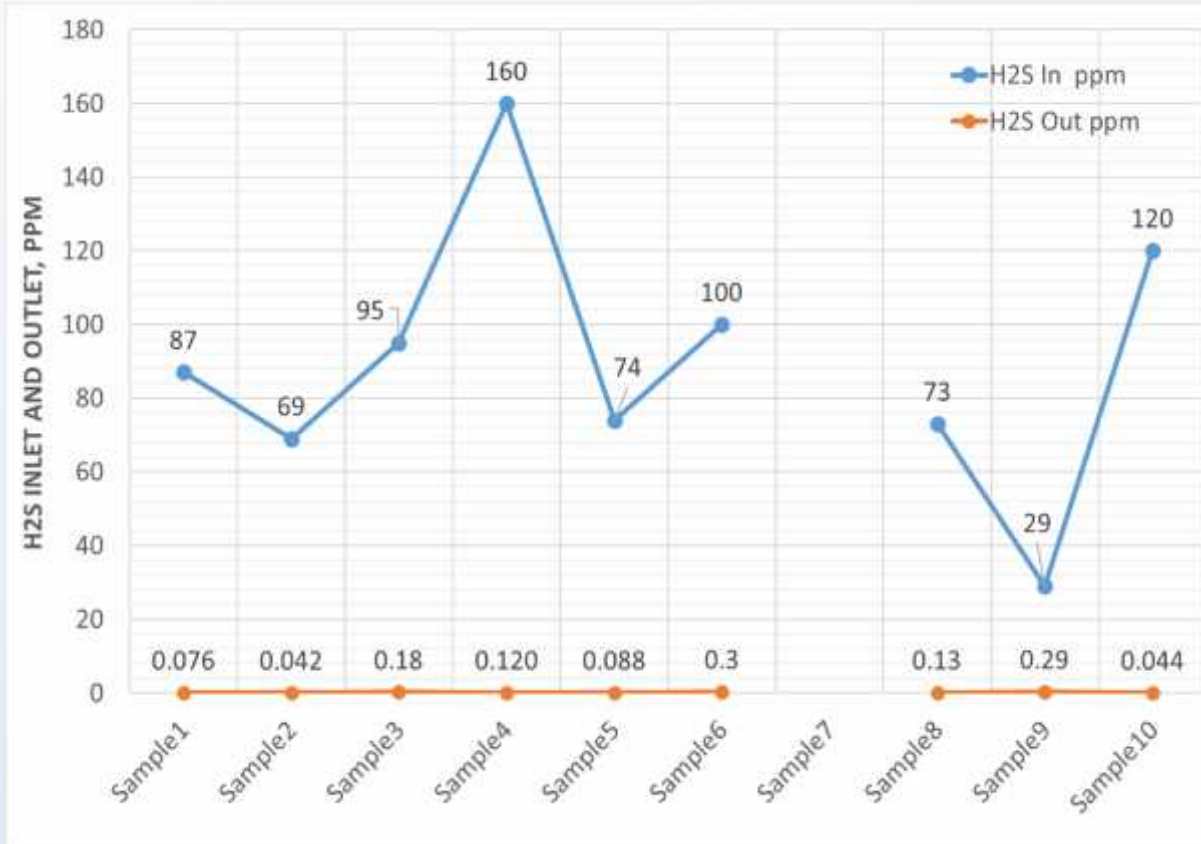


Digester Gas Sampling



- Raw gas samples (INLET) and
- Treated gas samples (OUTLET)
- Grab samples collected in pressurized Canisters analyzed for
 - Methane
 - CO₂
 - H₂S
- 30 min samples collected with Sorbent tubes and analyzed for
 - Siloxane

H₂S Removal Rate During the Pilot



- Average Inlet H₂S = 90 ppm
- Average Outlet H₂S = 0.14 PPM
- % H₂S Removal rate was 99.8 %

Siloxane Removal Rate During the Pilot



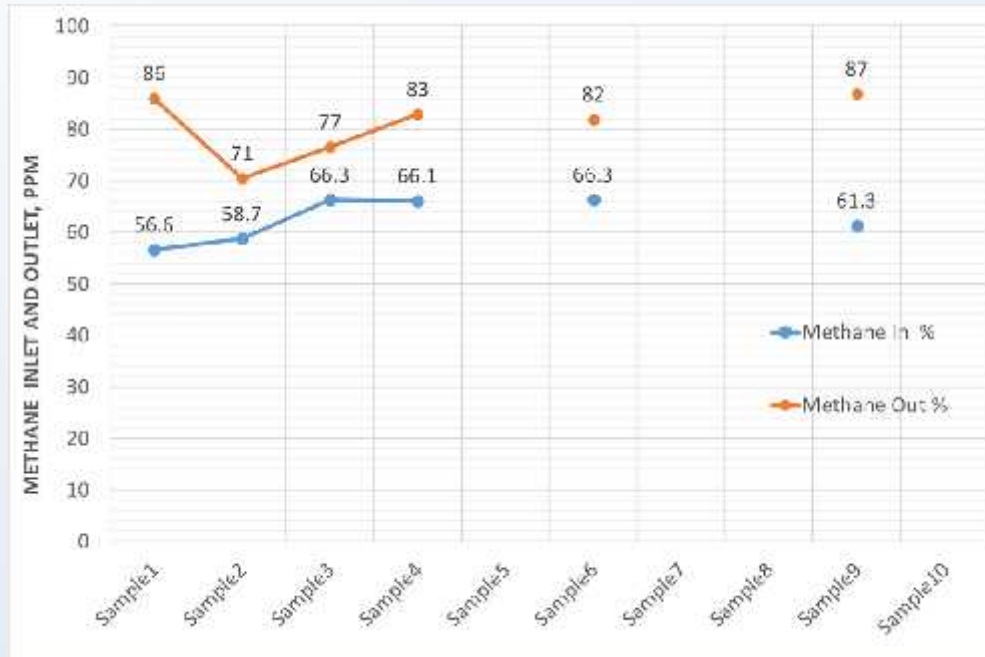
- Average Inlet Siloxane= 3,244 $\mu\text{g}/\text{m}^3$ as Si
- Average Outlet Siloxane = 1143 $\mu\text{g}/\text{m}^3$ as Si
- % Siloxane Removal rate 65%

CO₂ Removal Rate During the Pilot



- Average Inlet CO₂ = 32%
- Average Outlet CO₂ = 6%
- % CO₂ Removal rate 80%

Methane Surge During the Pilot



- Average Inlet CH_4 = 63%
- Average Outlet CH_4 = 81%
- % Methane Surge 29%

Pilot Unit Results

Parameter	Average Inlet Concentration	Average Outlet Concentration	Average Percent Change
H ₂ S (ppmV)	90	0.14	99.8% ± 0.3%
Siloxanes (ppmV as Si)	2.9	0.92	65% ± 13.6%
Methane (%)	63	81	29% ± 16%
Carbon Dioxide (%)	32	6.3	80.3% ± 14%

Challenges during the Pilot

- Too good to be true
- Plant Water Pressure and Flow impacts the treatment
- Gas pressure Fluctuation causes additional time in sampling

Preliminary Full Scale Estimate

- Pilot to be installed in the low pressure side
- Recommended gas pressure < 12 in H₂O
- For 1.3 MMCF gas production we need ~12 MGD plant water without recirculation (for MMSD)
- If we add water recirculation loop the anticipated water consumption can go down to $< \sim 6$ MGD
- In general 7 to 10 gpm per 1 scfm depending on available water pressure (without recirculation)

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Summary and Next Steps...

- Full scale pilot to be installed soon in Southern California
- Additional small scale “proof of concept” pilots around upper Midwest
- Refine water recycle loop which will reduce the inlet water requirement to the system
- Further improve methane quality in the product gas stream
- Collect additional data on various siloxane sources to better determine which species are efficiently removed using this process